

2014-11-07 Håvard Devold, ABB

Fra PID til Integrerte Operasjoner





1982

PID for ASEA MASTER PIECE

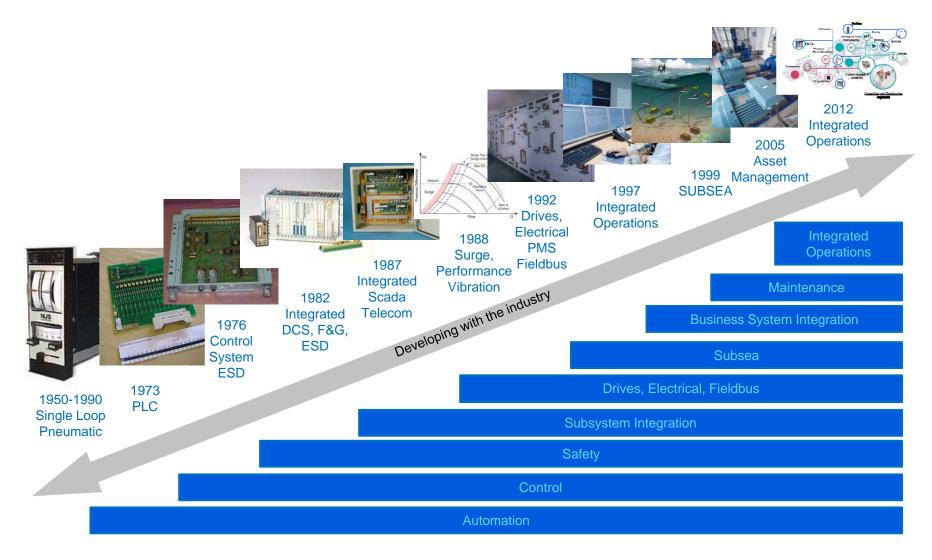






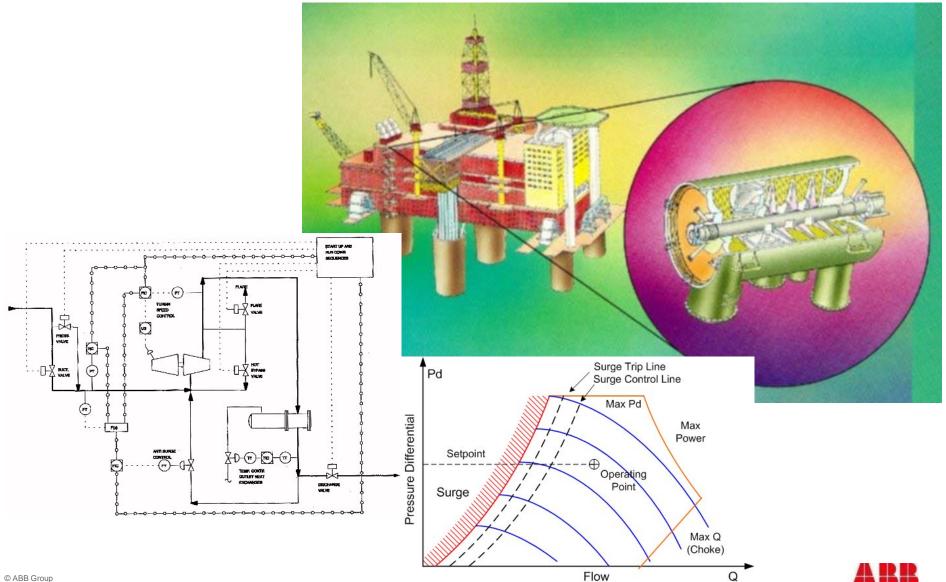
© ABB Group November 17, 2014 | Slide 2

Automation and Control Evolution



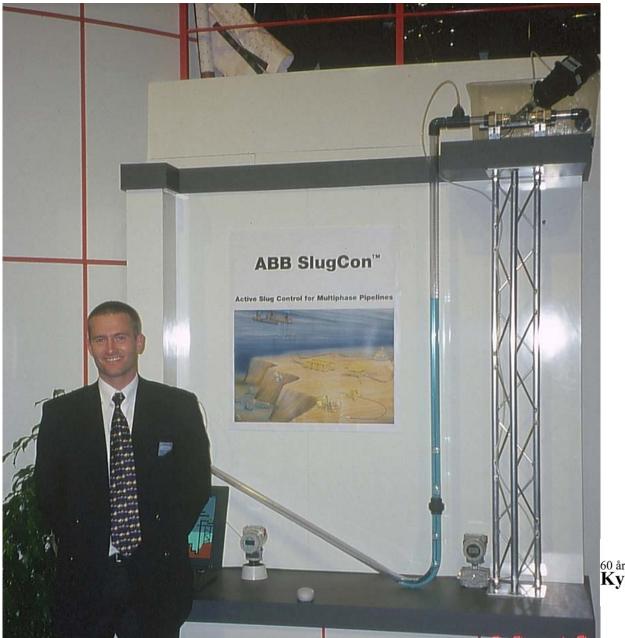


1992 – Compressor Control



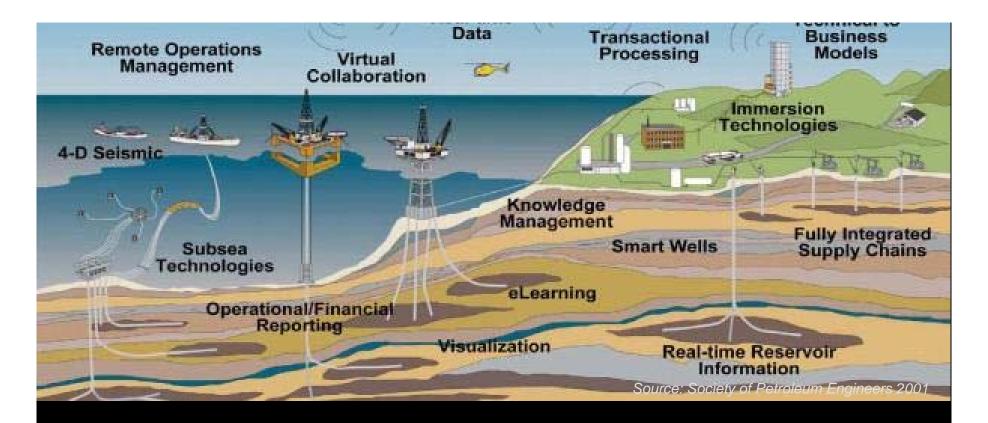
© ABB Group November 17, 2014 | Slide 4





© ABB Group November 17, 2014 | Slide 5



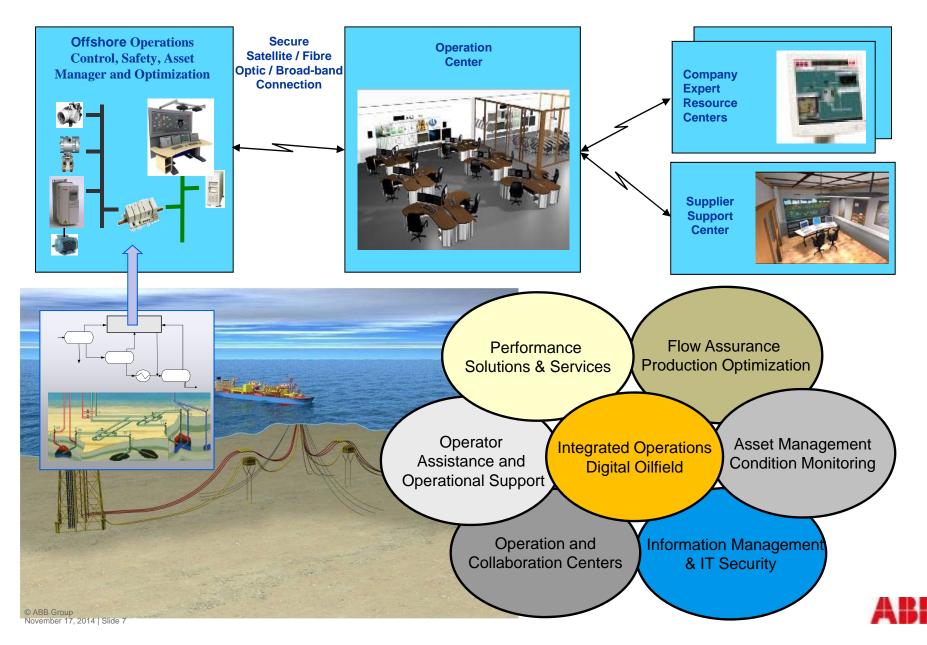


InSegrerte Operasjoner Digital Oilfield

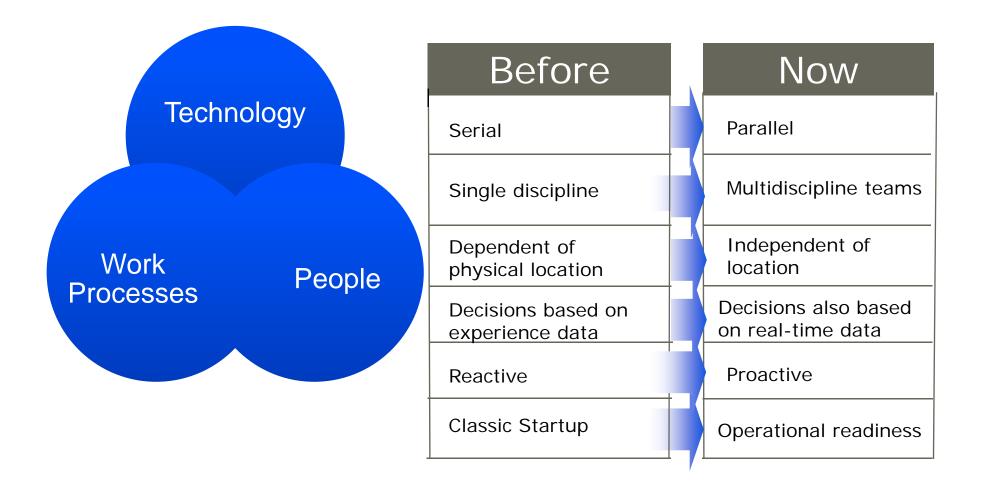




Digital Oilfield Structure

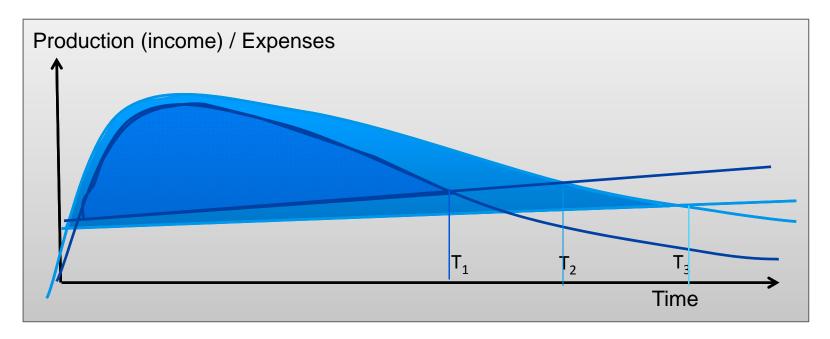


Integrated operations Safe, better and faster decisions





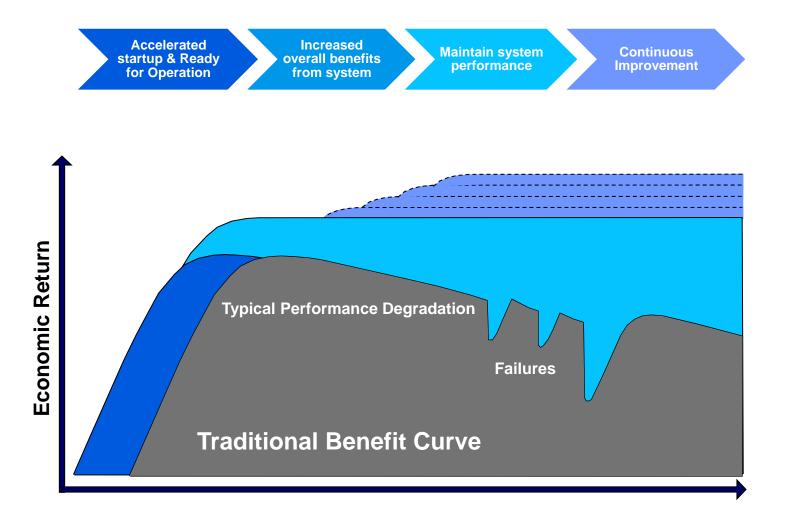
Digital Oilfield: Value Potential



- Increased production (3-5%)
- Reduced production losses (20-40%)
- Reduced operation and maintenance costs (15-30%)

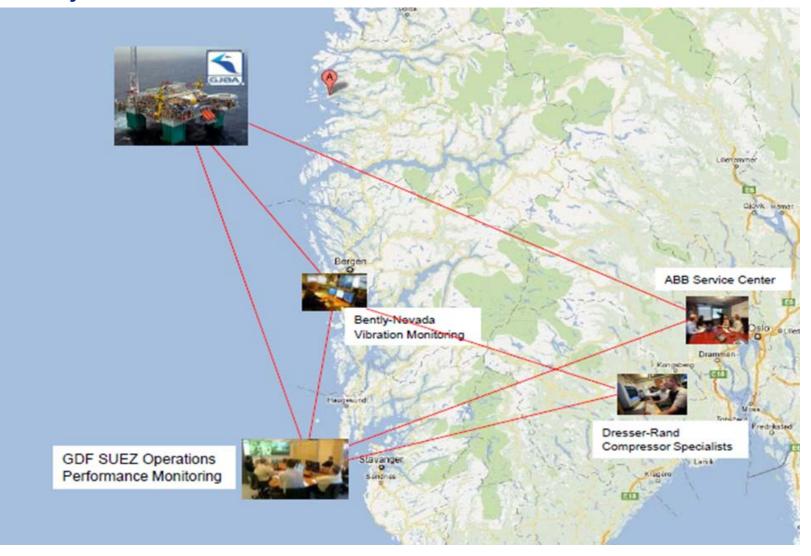


EICT Life-cycle service The target





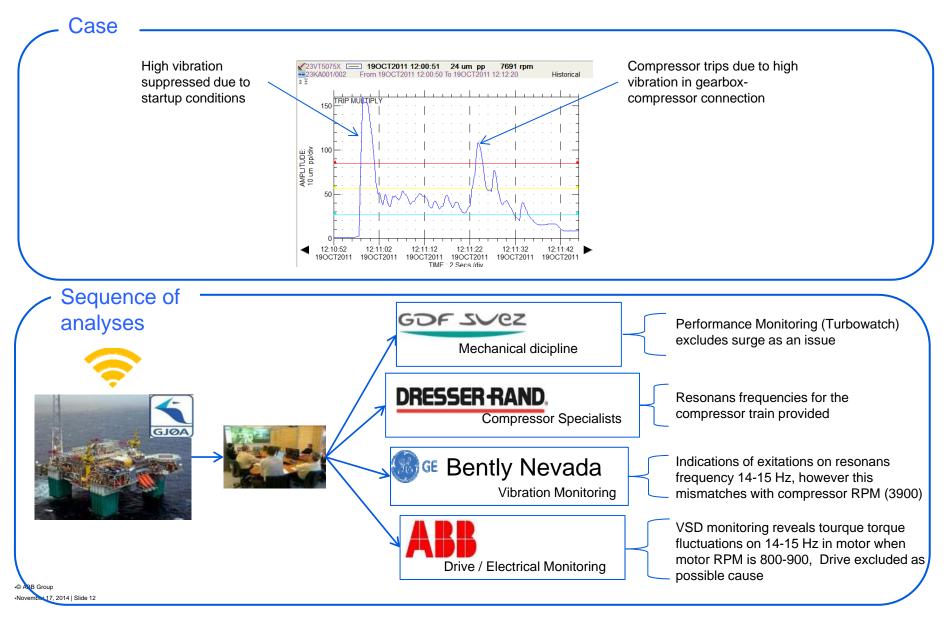
How remote condition monitoring improve availability FPU Gjøa





Operational flexibility

Case: GDF SUEZ, Compressor tripping on high vibration



Operational flexibility

Case: GDF SUEZ, Compressor tripping on high vibration

Root cause and solution

- Trip caused by vibrations in 14-15 Hz regime
- Resonance frequency of the compressor train in 14-15 Hz domain
- Resonance frequency exited when motor RPM is 800-900
- Detection of critical rotation speed via the VSD monitoring analyzing torque fluctuations
- Solution:
 - Fast acceleration through the critical rotation speed interval
 - Trip-multiply implemented from onshore location
- Result
 - Minor changes in the protection system eliminate the problem. The platform can continue operating with minimal downtime

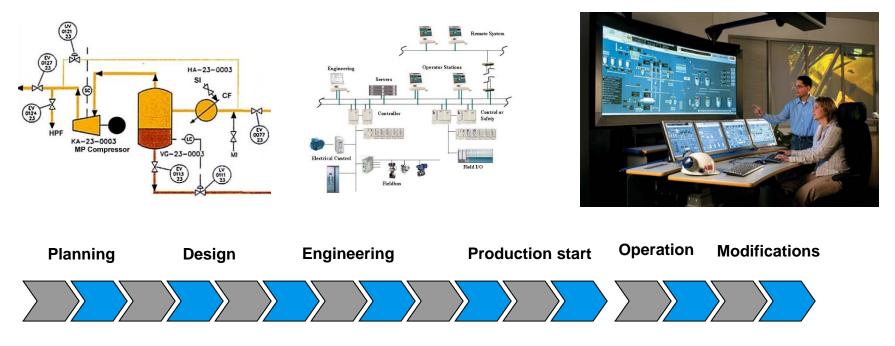
Enablers

7. 2014 | Slide 13

- GFD SUEZ strategy for Integrated Operations, C097-AKE-A-FD-0013, Integrated Operation Strategy:
 - · "Based on criticality classification, all equipment and systems shall be designed for real time condition monitoring."
 - "The data shall be made available both onshore and offshore using high quality data/information transfer"
- GFD SUEZ Operational philosophy
- Access to information for internal and external users and extensive use of service partners
- Instrumentation to cater for condition based maintenance as a part of the project delivery
- · All relevant parameters for the compressor was monitored:
 - The process conditions and performance
 - Vibration analyzes
 - The electrical parts of the system monitored as a part of the compressor solution.
- ABB service Environment[™] provided easy accsess to experts for discussions, analyzes, data collection and problem solving.



Lifecycle simulator



Design & Engineering Simulator

Control System Test

Operator Training Simulator

Training of new operators, hazard training

Process optimization and modification studies



Process Perforance Case: Problem description Design objective

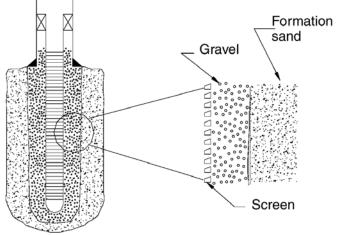
Who Where What How Results Conclusion The wells at Ormen Lange are completed with a gravel pack. An increase in the gas rate must be slow and controlled in order to avoid disturbances in the natural pack.

Design objective:

Protect the integrity of the wells:

- Keep pressure drops less than 4 bar/h
- Keep drawdown less than 25 bar
- Keep flow rate less than 10 MSm3/d

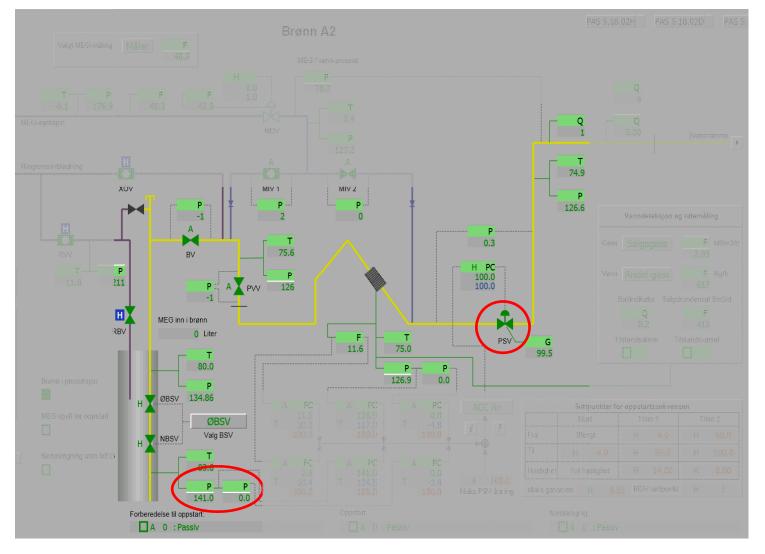
This was previously solved by: Assuming worst-case conditions and opening the valve with a predefined, fixed speed.





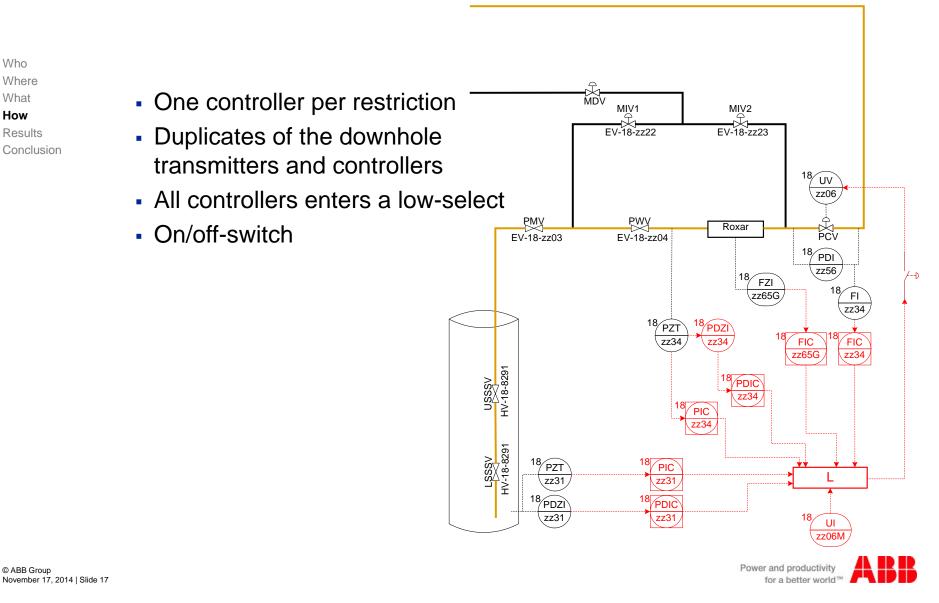
Problem description Instrumentation and valves







Solution details Implemented control solution



Solution details Tuning of controllers

Who Where What How Results Conclusion

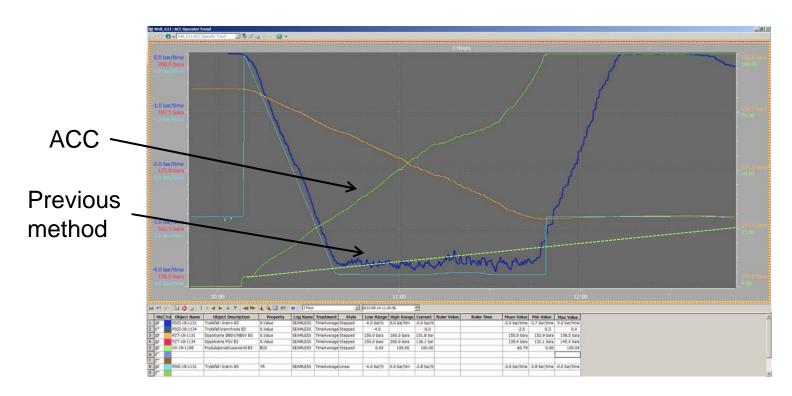
- We created a model that estimates the process behavior, based on:
 - The opening of the choke valve
 - The pressure-drop over the valve
- We implemented Skogestad's tuning-rules in the control system
 - The tuning of the controllers are dynamically updated, based on the estimated process behavior



Customer value A side-effect of the solution: Much quicker startup

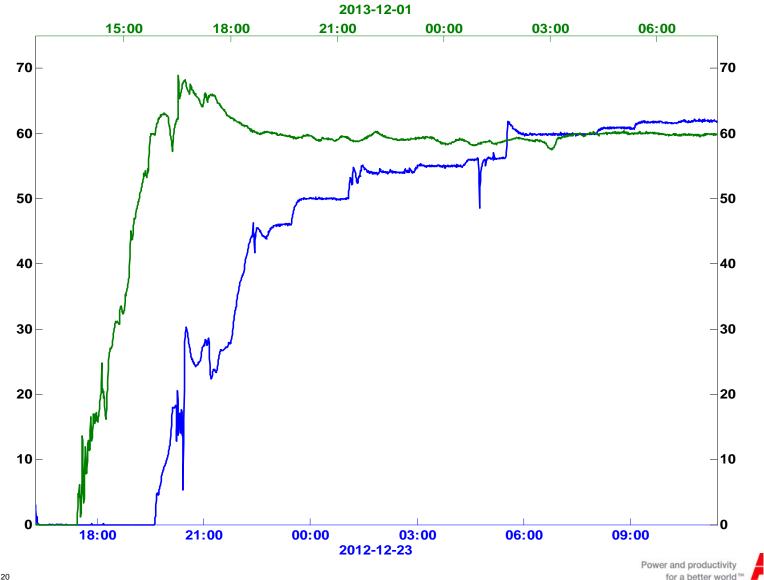
Who Where What How Results Conclusion

- Ramp-up of well B3, with aggressive tuning
- ACC used 1 hour and 40 minutes to ramp-up the well
- Previously would have used 9 hours



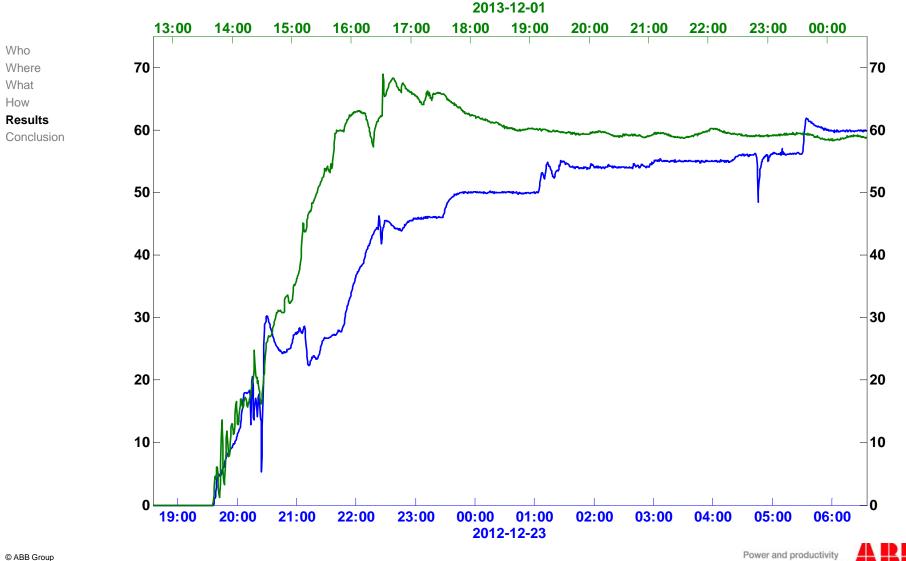


Comparison of flow rates Difference is approx. 10 MSm3



© ABB Group November 17, 2014 | Slide 20

Comparison of flow rates Difference is approx. 5 MSm3



for a better world™

© ABB Group November 17, 2014 | Slide 21

Customer value What is this worth for Shell?

Who Where What How Results **Conclusion** Production loss:

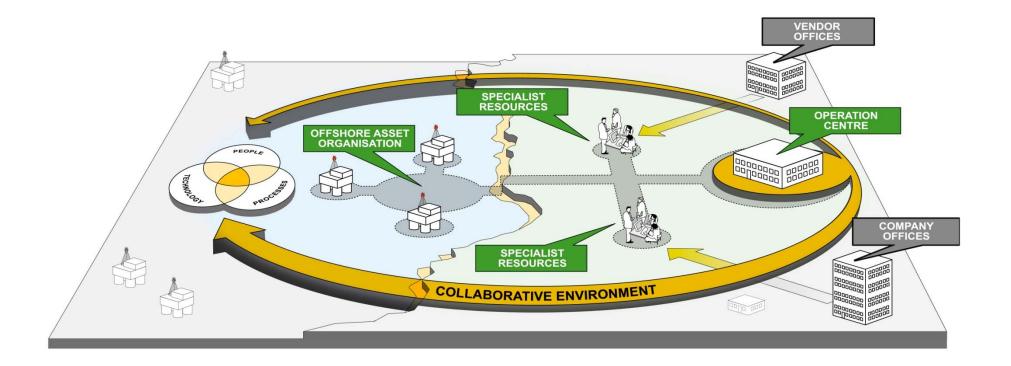
- All the wells have to be shut down 2 times per year, due to integrity testing
- If the onshore facility goes down, the wells have to be shut down within 30-60 minutes

Customer value:

- Previously, a ramp-up of a high-pressure well took 15-20 hours (up to 30 for some new wells)
- With ACC, the same well takes 4.5 hours
- The gained production is 5-10 MSm³, per plant startup
- For high-pressure wells: Can be as high as 1MSm³ per well per startup



ABB Integrated Operations From technical to operational integration





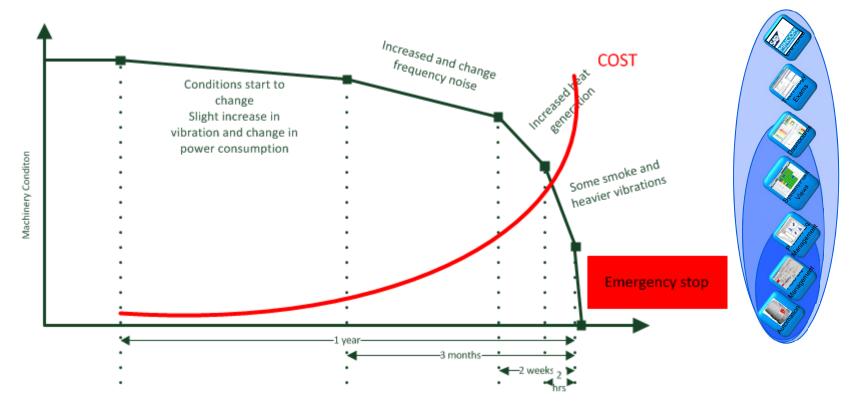
Integrated Operations Structured Safety and Alarm Management

龤 Alarm Manager vsis Alarm Change History Block Log Alarm and Event Log Site Actions View All Site Content Alarm Manager Frequent Alarms Lists Performance Level Successful alarm management ensures optimal working conditions for operators while ensuring safe and predictable alarm and safety system Discuss Description Numbe Name havior Sites G35XB___6106A GW MCS ModemPair X/Y 9132 People and Groups The Alarm Manager provides a complete toolset for operators and alarm G35XB___6106B RS MCS ModemPair X/Y 8856 Recycle Bin C11LA___0032_ experts, ensuring plant integrity and meeting government requirements and industry guidelines. This product is part of the Integrated Operations SJEKK C11LT___0032 6111 100 Level 2 Reactive U86XB___6124A HP Duty Pump Permiss 3237 portfolio U86XB___6124B LP Duty Pump Permiss 1764 W21XB___1072_ FILT.A BW I DRIFT 1029 10 An alarm system should release an alarm only when the plant condition requires Level 3 Stable W21XB 2072 FUT B BW I DRIFT 1029 operator action. However, most alarm systems are not optimally configured W21XB____3072_ FILT.C BW I DRIFT 1026 which leads to both insufficient alarming and a high number of nuisance alarms. W21XB____4072_ FILT.D BW I DRIFT 1023 As a result, the operator stress and work load increases significantly. A51XB___8621A D1 LP SUP INTERLOCK 846 The Alarm Manager is the ideal tool for day to day follow-up of an alarm system A51XB___8628A E2 LP SUP INTERLOCK 786 as well as being a toolset well suited for alarm system improvement projects. A51XB___8622A D2 LP INTERLOCK 750 10 100 1000 K11NGB 6520E KRAN I DRIFT 627 Government regulations as well as company internal alarm philosophy require A21LICA_0190_ 1ST SEP.TRAIN2 VANN 618 documentation of current alarm system status and fully documented alarm Top 10 load: 92.93% A51XB___8623A D3 LP INTERLOCK 594 system design. The Alarm Manager helps keeping track of the alarm system Top 20 load: 99.66% Avarage rate (avg): 71 alarms/h Standing alarms: 142 Time in upset condition: 12% A51XB___8629A E3 LP INTERLOCK 564 status, improving performance, and automating mandatory reports. W22XZY___2202B WI P200 FELLES AL 558 The Alarm Manager is compliant with the standards EEMUA 191, YA-711, and A51XB___8627A E1 LP SUP INTERLOCK 531 ISA 18.02 A41KJI__0103A LINE MAX FLOW T.SEP 498 G35XA 6115A Modem Pair1 Line A 495 Initiated Alarms Max value: 9267 Number of Alarms: 133116 Average: 964.61 InitiatedAla Inter (HALINE) Pages Renchma 10000 **Results** - Filtering 8000 279 1611 279 1621 271 160 271 160 271 160 201019034 201019011 201019022 201019024 20100041 20100041 6000 4000 2000 0 2010-02-07 2010-02-21 2010-03-07 2010-03-21 2010-04-04 2010-04-18 2010-05-02 2010-05-16 2010-05-1 StonTime



the second second

Integrated Operations Realizing the value of a modern maintenance strategy

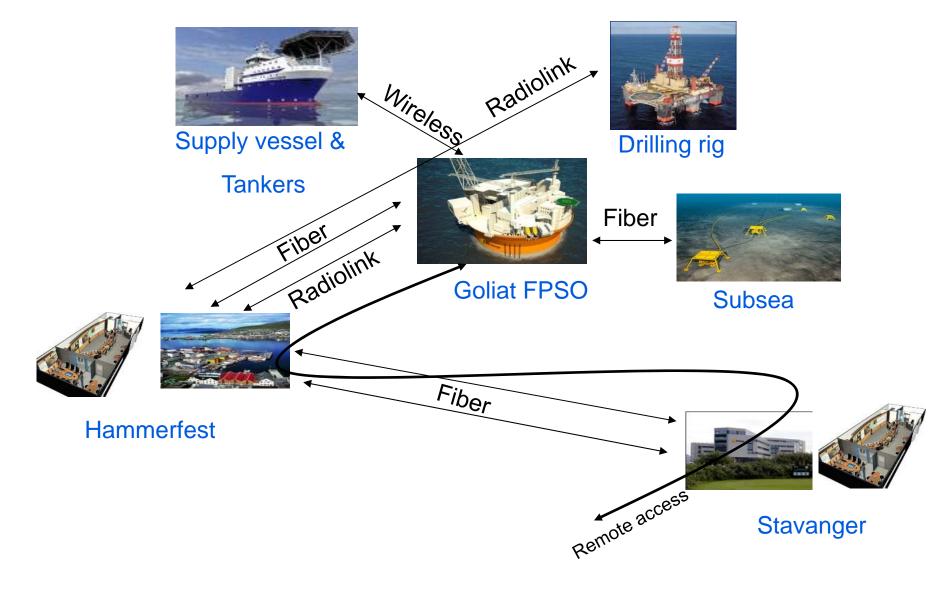


An active maintenance strategy with structured work process and modern tools enables early fault detections, reduces costs and avoids expensive breakdowns





Digital Oilfield Topology





Power and productivity for a better world[™]

